

An innovative phase transition modeling for reproducing cavitation through a five-equation model and theoretical generalization to six and seven-equation models

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Maria Giovanna Rodio, Rémi Abgrall. An innovative phase transition modeling for reproducing cavitation through a five-equation model and theoretical generalization to six and seven-equation models. [Research Report] RR-8664, INRIA Bordeaux; INRIA. 2015. <hal-01100706v2>

HAL Id: hal-01100706

<https://hal.inria.fr/hal-01100706v2>

Submitted on 15 Jan 2015

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An innovative phase transition modeling for reproducing cavitation through a five-equation model and theoretical generalization to six and seven-equation models

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**RESEARCH
REPORT**

N° 8664

January 2015

Project-Teams Cardamom



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Research Report n° 8664 — January 2015 — 36 pages

Abstract: This work is devoted to model the phase transition for two-phase flows with a mechanical equilibrium model. First, a five-equation model is obtained by means of an asymptotic development starting from a non-equilibrium model (seven-equation model), by assuming a single-velocity and a single pressure between the two phases, and by using the Discrete Equation Method (DEM) for the model discretization. Then, a splitting method is applied for solving the complete system with heat and mass transfer, *i.e.*, the solution of the model without heat and mass transfer terms is computed and, then, updated by supposing a heat and mass exchange between the two phases. Heat and mass transfer is modeled by applying a thermo-chemical relaxation procedure allowing to deal with metastable states.

The interest of the proposed approach is to preserve the positivity of the solution, and to reduce at the same time the computational cost. Moreover, it is very flexible since, as it is shown in this paper, it can be extended easily to six (single velocity) and seven-equation models (non-equilibrium model).

Several numerical test-cases are presented, *i.e.* a shock-tube and an expansion tube problems, by using the five-equation model coupled with the cavitation model. This enables us to demonstrate, using the standard cases for assessing algorithms for phase transition, that our method is robust, efficient and accurate, and provides results at a lower CPU cost than existing methods. The influence of heat and mass transfer is assessed and we validate the results by comparison with experimental data and to the existing state-of-art methods for cavitation simulations.

Key-words: Heat and mass transfer, two-phase flows, Discrete Equation Method (DEM), seven-equation model, six-equation model, five-equation model, cavitation.

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Un modèle de transition innovant pour simuler la cavitation à travers un modèle à 5 équations, et généralisation aux modèles à 6 et 7 équations

Résumé : Ce travail est focalisé sur un modèle de transition de phase pour des écoulements diphasiques avec un modèle d'équilibre mécanique. Premièrement, un modèle à 5 équations est obtenu avec un développement asymptotique à partir d'un modèle à 7 équations, en supposant une seule vitesse et pression pour les deux phases, et en utilisant une méthode DEM (Discrete Equation Method) pour la discrétisation du modèle. De plus, une méthode de splitting est appliquée pour résoudre le système complet avec transfert de masse et de chaleur. Donc, la solution du modèle sans transfert de masse et de chaleur est calculée et mise à jour en supposant un transfert de masse et de chaleur. Le transfert de masse et chaleur est modélisé en appliquant une procédure de relaxation thermo-chimique permettant de traiter des états métastables. L'intérêt de cette approche est de préserver la positivité de la solution, et de réduire le coût de calcul. De plus, elle est très flexible et peut facilement être étendue à des modèles à 6 et 7 équations. Plusieurs cas-tests sont présentés, un tube à choc et un tube de détente, en utilisant un modèle à 5 équations couplé avec un modèle de cavitation. Cela permet de démontrer que notre méthode est robuste, précise et fournit des résultats avec un coût de calcul réduit par rapport aux méthodes existantes. L'influence du transfert de masse et de chaleur est estimée en comparant les données expérimentales avec des résultats existants en littérature.

Mots-clés : transferts de masse et de chaleur, écoulements diphasiques, DEM, modèles à 7 équations, modèles à 6 équations, modèles à 5 équations, cavitation.

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1 Introduction

Modeling the heat and mass transfer between the phases is of utmost importance when simulating flows in fuel injectors, turbo-pumps, nozzles, etc. Usually, in some of these applications, cavitation could appear because of a strong liquid acceleration, yielding a strong rarefaction wave and hence with vapor/gas bubbles creation. In Fig. 1, the pressure-volume diagram is illustrated. The dashed line (from ‘saturated liquid’ to ‘saturated vapor’ in Fig. 1) is the saturation curve, where the two phases are characterized by the same pressure, temperature and chemical potential. Following [1, 2], let us assume the liquid phase evolves following the isotherm line (solid line), from the state A to the state B. If it is depressurized to a pressure below the corresponding saturation pressure of state B, it can evaporates, moving on the isothermal line (arriving to C), up to the equilibrium condition in the gas monophasic region (for example in state E) (see

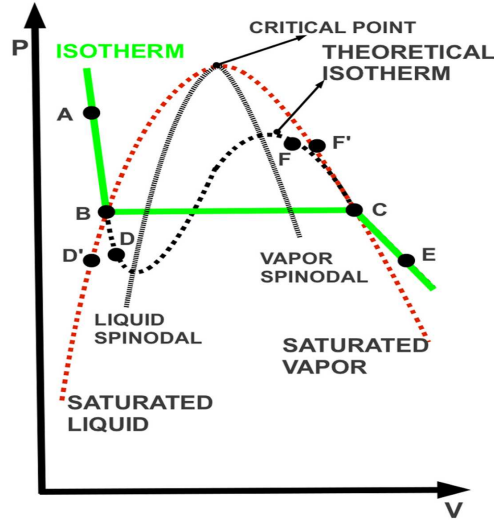


Figure 1: Pressure-volume diagram

[1] for more details). However, if the liquid undergoes a very strong rarefaction wave, it can evolve from the state A to a 'metastable' state (state D), i.e. a non-equilibrium state. This means that, in these conditions, the liquid phase releases its metastable energy, producing vapor and, thus, evolving in a new equilibrium state (for example in state E). The consequences of cavitation, such as noise, performance device reduction and wall corrosion, are extremely negative. For these reasons, this phenomenon requires a good theoretical comprehension and, as consequence, an accurate predictive physical model is required.

In the literature, several numerical models have been proposed for reproducing the two-phase flows. The most used are (i) the *Bubbly Flow Models* [3, 4, 5, 6], (ii) the *Homogeneous Mixture Models* [7, 8, 9, 10, 11] and (iii) the *Multiphase Models* [12, 13, 14, 15, 16]. The main difference, among these families of models, consists in the assumptions for modeling the interaction and the behavior of the two phases.

In this paper, the focus is on the *Interface diffuse Models*. In one dimension, they consist in a system of three conservation equations for each phase and a transport equation for the vapor fraction. This system enables the explicit treatment of the mass, momentum and energy exchanges as transfer terms.

However, these models are numerically complex, and more recent works have proposed the introduction of relaxation procedures to reduce the system to five equations, ensuring the possibility of dealing with explicit mass and energy exchange [17, 18, 15]. The most important reference about the treatment of heat and mass transfer terms, for the Interface Diffusive models, is the work of Saurel et al. [19]. The authors proposed a phase transition modeling for a single velocity and single pressure model (five equations model) relying on a thermo-chemical relaxation. In fact, by obtaining the equality of temperature and chemical potential for the two phases, this relaxation assures the evolution

of liquid phase from a metastable state to an equilibrium state on the saturation curve. During this evolution, the liquid phase releases mass in order to evaporate before assuming a new state on the saturation curve. Then, the authors proposed an original procedure to identify the liquid/vapor interface. In recent years, few works have been proposed for treating phase transition modeling in Interface Diffusive models [16, 19, 20, 21, 22, 23, 24]. Following the approach of [19], Zein et al. [20] proposed a heat and mass transfer model for the six equation system (single velocity model), based on three different relaxations of pressure, temperature and chemical potential, respectively. Recently, the same approach has been used by Wang et al. in [23] and Daude et al. [22]. Nevertheless, the original relaxation procedure of [19] and the successive modifications are affected by some numerical issues. In order to preserve the positivity of volume fraction and density, it might be necessary to integrate the system using time steps that are fractions of the hydrodynamic time step, thus yielding an increase of the computational cost (see [20]). Recently, Pelanti and Shyue [21] presented a new numerical treatment of heat and mass transfer terms for a six equation two-phase model. As in [25], they proposed, in an original way, a new procedure in order to guarantee the positivity of the system, based on the total entropy maximization, when the solution coming from the thermo-chemical relaxation step, is not physically admissible.

The first idea of the present paper is to couple the treatment of heat and mass transfer terms proposed in [19] for a five equation model, with the procedure for solution admissibility of [21], thus preserving the positivity of the solution and reducing consistently the computational cost. As a consequence, this method combines a good accuracy and a reduced computational cost, as demonstrated in the following by performing several comparisons with experimental data and other numerical results well-known in the literature. The second innovative point of this work is the theoretical extension of the proposed model to six and seven-equation models, thus showing its flexibility.

The paper is organized as follows. Section 2 presents the five-equation model with heat and mass transfer starting from a seven-equation one. Section 3 illustrates the main ingredients of the proposed approach for simulating cavitating flows. In Section 5, a theoretical extension of the cavitation model to the six and seven-equation model is presented and discussed. Section 6 illustrates several numerical results obtained with the five-equation model, displaying the robustness of the numerical method on the most used numerical configuration in the literature. In particular, the influence of heat and mass transfer is assessed and the results are validated by comparison with respect to the experimental data.

Finally, in Section 7, some conclusions and perspectives are drawn.

2 The five-equation models with heat and mass transfer

We introduce here the general formulation of a seven-equation model and the assumptions for yielding a five equations models, with heat and mass transfer

[20]:

$$\begin{aligned}
\frac{\partial \alpha_1}{\partial t} + v_I \frac{\partial \alpha_1}{\partial x} &= \mu(P_1 - P_2) + \eta Q + \frac{\rho}{\rho_I} \dot{Y} \\
\frac{\partial(\alpha_1 \rho_1)}{\partial t} + \frac{\partial(\alpha_1 \rho_1 v_1)}{\partial x} &= \rho \dot{Y} \\
\frac{\partial(\alpha_1 \rho_1 v_1)}{\partial t} + \frac{\partial(\alpha_1 \rho_1 v_1^2 + \alpha_1 P_1)}{\partial x} &= P_I \frac{\partial \alpha_1}{\partial x} + \lambda(v_2 - v_1) + v_I \rho \dot{Y} \\
\frac{\partial(\alpha_1 \rho_1 E_1)}{\partial t} + \frac{\partial(\alpha_1(\rho_1 E_1 + P_1)v_1)}{\partial x} &= P_I v_I \frac{\partial \alpha_1}{\partial x} + \lambda v_I(v_2 - v_1) + \\
&\quad + \mu P_I(P_1 - P_2) + Q + E_I \rho \dot{Y} \quad (1) \\
\frac{\partial(\alpha_2 \rho_2)}{\partial t} + \frac{\partial(\alpha_2 \rho_2 v_2)}{\partial x} &= -\rho \dot{Y} \\
\frac{\partial(\alpha_2 \rho_2 v_2)}{\partial t} + \frac{\partial(\alpha_2 \rho_2 v_2^2 + \alpha_2 P_2)}{\partial x} &= P_I \frac{\partial \alpha_2}{\partial x} - \lambda(v_2 - v_1) - v_I \rho \dot{Y} \\
\frac{\partial(\alpha_2 \rho_2 E_2)}{\partial t} + \frac{\partial(\alpha_2(\rho_2 E_2 + P_2)v_2)}{\partial x} &= P_I v_I \frac{\partial \alpha_2}{\partial x} - \lambda v_I(v_2 - v_1) + \\
&\quad - \mu P_I(P_1 - P_2) - Q - E_I \rho \dot{Y},
\end{aligned}$$

where:

- $Q = \theta(T_2 - T_1)$ is the heat transfer term, T_2 and T_1 are the liquid and the gas temperature, respectively
- $\dot{Y} = \nu(g_2 - g_1)$ is the mass transfer term, g_2 and g_1 are the liquid and the gas Gibbs free energy, respectively.

The symbols ρ_k , α_k , v_k and P_k represent the density, the volume fraction, the velocity and the pressure for each phase, respectively. The terms ρ_I , E_I , P_I and v_I are the density (see Eq. (10)), the energy (see Section 5.1.4), the pressure and the velocity (see Section 5.1.2) at the interface, respectively. Last, $\rho = \alpha_1 \rho_1 + \alpha_2 \rho_2$ is the mixture density. The coefficients $\lambda = C/\varepsilon$ and $\mu = C'/\varepsilon$ represent the relaxation velocity parameter and the dynamic compaction viscosity. The coefficients C and C' depend on the acoustic impedance of the fluids (see [26] for more details). These are the so-called *relaxation terms*, which yield a process inducing a pressure and velocity equilibrium.

The system (1) can be, also, expressed in vectorial form as follows:

$$\frac{\partial U}{\partial t} + \frac{\partial}{\partial x} F(U) + B(U) \frac{\partial \alpha_1}{\partial x} = \frac{R(U)}{\varepsilon} + S(U) \quad (2)$$

where

$$U = \begin{pmatrix} \alpha_k \\ \alpha_k \rho_k \\ \alpha_k \rho_k v_k \\ \alpha_k \rho_k E_k \end{pmatrix}, \quad F(U) = \begin{pmatrix} 0 \\ \alpha_k \rho_k v_k \\ \alpha_k (\rho_k v_k^2) + P_k \\ \alpha_k (\rho_k E_k + P_k) v_k \end{pmatrix}$$

$$B(U) = \begin{pmatrix} v_I \\ 0 \\ -P_I \\ -P_I v_I \end{pmatrix}, \quad \frac{R(U)}{\varepsilon} = \begin{pmatrix} \mu(P_k - P_{k^*}) \\ 0 \\ \lambda(v_{k^*} - v_k) \\ \lambda v_I \cdot (v_{k^*} - v_k) - \mu P_I (P_k - P_{k^*}) \\ -\mu(P_1 - P_2) \end{pmatrix}, \quad \text{Inria}$$

$$S(U) = \begin{pmatrix} \frac{\alpha_1 \alpha_2}{\alpha_2 \rho_1 c_1^2 + \alpha_1 \rho_2 c_2^2} \left(\frac{\Gamma_1}{\alpha_1} + \frac{\Gamma_2}{\alpha_2} \right) Q + \frac{\rho}{\rho_I} \dot{Y} \\ \rho \dot{Y} \\ v_I \rho \dot{Y} \\ Q + E_I \rho \dot{Y} \end{pmatrix}.$$

In order to reduce the complexity of the system, mechanical equilibrium is considered. The equality of pressure and velocity can be obtained through a stiff mechanical relaxation of the system (1), as in [27, 21, 20], or through an asymptotic development, as in [28, 15], where relaxation parameters, λ and μ , are assumed as tending to infinity. This means that a very large interface area is assumed. After a Chapman-Enskog like expansion, the system (1) becomes:

$$\begin{aligned} \frac{\partial \alpha_1}{\partial t} + v \frac{\partial \alpha_1}{\partial x} &= K \frac{\partial v}{\partial x} + \eta Q + \frac{\rho}{\rho_I} \dot{Y} \\ \frac{\partial \alpha_1 \rho_1}{\partial t} + \frac{\partial (\alpha_1 \rho_1 v)}{\partial x} &= \rho \dot{Y} \\ \frac{\partial \alpha_2 \rho_2}{\partial t} + \frac{\partial (\alpha_2 \rho_2 v)}{\partial x} &= -\rho \dot{Y} \\ \frac{\partial \rho v}{\partial t} + \frac{\partial (\rho v^2 + P)}{\partial x} &= 0 \\ \frac{\partial \rho E}{\partial t} + \frac{\partial (\rho E + P)v}{\partial x} &= 0, \end{aligned} \quad (3)$$

where $E = e + \frac{1}{2}v^2$ is the mixture total energy and $e = (\alpha_1 \rho_1 e_1 + \alpha_2 \rho_2 e_2)/\rho$ is the mixture internal energy. $K = \frac{\alpha_1 \alpha_2 (\rho_2 c_2^2 - \rho_1 c_1^2)}{(\alpha_1 \rho_2 c_2^2 + \alpha_2 \rho_1 c_1^2)}$. The unknowns are now : α_1 , ρ_k , v , P , e_k , Q and \dot{Y} . This means that, for closing the system, two equations of state are used for defining the relation of energy as a function of pressure and density for both phases (see Section 4) and a cavitation model is used in order to define Q and \dot{Y} . This is detailed in Section 3.

3 The cavitation model for the five-equation model: a splitting method

Now, let us consider the system (3). In order to compute a solution, a splitting procedure is adopted and the following three steps are solved:

- *Step 1*: compute the numerical solution of the hyperbolic part of system (3) without heat and mass transfer term source.

Three strategies are possible. The first one is to solve the five equation model directly, as in [19]. The second possibility is to solve the seven equation model (system (1)) without the heat and mass transfer terms and, then, to apply a mechanical relaxation in order to obtain the pressure and velocity equilibrium.

The third possible strategy is the one used in this work. It consists in following the procedure used in [14, 18], *i.e.* the discrete equation method (DEM) [29] applied to the system (1). An advantage to use the DEM method for (2) is an original way of addressing a important numerical

challenge: the approximation of non-conservative term, when the velocity \vec{v} and K are simultaneously discontinuous (see [29, 18, 26] for more details).

Then, an asymptotic development is applied, at a discrete level, in order to impose to the semi-discrete system a mechanical relaxation. Finally, a final semi-discrete system is obtained, that is equivalent to discretize the five equation model (3).

- *Step 2*: update the solution of system (3), by solving the temporal ODEs system with the heat and mass transfer terms. This consists in applying a thermo-chemical relaxation that allows, from a metastable state, to attain a new equilibrium solution.
- *Step 3*: the thermo-chemical relaxation does not guarantee that the positivity of the solution be preserved, so a positivity check of the solution is performed.

As explained in Section 1, a thermo-chemical relaxation is required in order to compute a new equilibrium state.

By adopting the splitting method, it is assumed that the characteristic time of a mechanical relaxation, $1/\mu$, is much smaller than the characteristic time scales $1/\theta$ and $1/\nu$ of heat and mass transfer terms, respectively. This means that thermal and chemical relaxation occur in a pressure equilibrium condition. In Fig. 2, the three steps are summarized in order to give a more complete vision of the global method.

In the following sections, the three steps are described in detail.

3.1 Step 1: Numerical solution of a five-equation model with mechanical relaxation without heat and mass transfer

The originality of this work is focused on the transition phase, thus for the step 1, only the main lines of the numerical method, proposed in [18], are recalled.

We assume that at time t , the computational domain Ω is divided into the cells $\mathcal{C}_i =]x_{i-1/2}, x_{i+1/2}[$. At a time $t = t + s$ (with s small), the interface in $x_{i+1/2}$ moves at a velocity $\sigma_{i+1/2}$ and the interface in $x_{i-1/2}$ moves at a velocity $\sigma_{i-1/2}$. As a consequence, the cell \mathcal{C}_i evolves in $\bar{\mathcal{C}}_i =]x_{i-1/2} + s\sigma_{i-1/2}, x_{i+1/2} + s\sigma_{i+1/2}[$ (see Fig. 3). The cell may be either smaller or larger than the original ones \mathcal{C}_i , depending on the signs of the velocities. So, the Godunov scheme [30] is no longer applied on the mesh cells, but on the modified and non-uniform cells constructed according to the position of the interface (see Fig. 3). Then, we introduce the characteristic function X^k of the phase Σ_k . The function $X^k(x, t)$ is equal to 1, if x lies in the fluid Σ_k at time t and 0 otherwise. Then, we denote with $F(U_L, U_R)$ the Godunov numerical flux between the states U_L and U_R , and with $F^{lag}(U_L, U_R)$ the flux across the contact interface between the states U_L and U_R (see Fig. 3). The relation between the two fluxes is equal to :

$$F^{lag}(U_L, U_R) = F(U_{LR}^+) - \sigma(U_L, U_R)U_{LR}^+ = F(U_{LR}^-) - \sigma(U_L, U_R)U_{LR}^-, \quad (4)$$

where the superscripts \pm denote the state on the right and on the left of the contact discontinuity, as in Fig. 3.

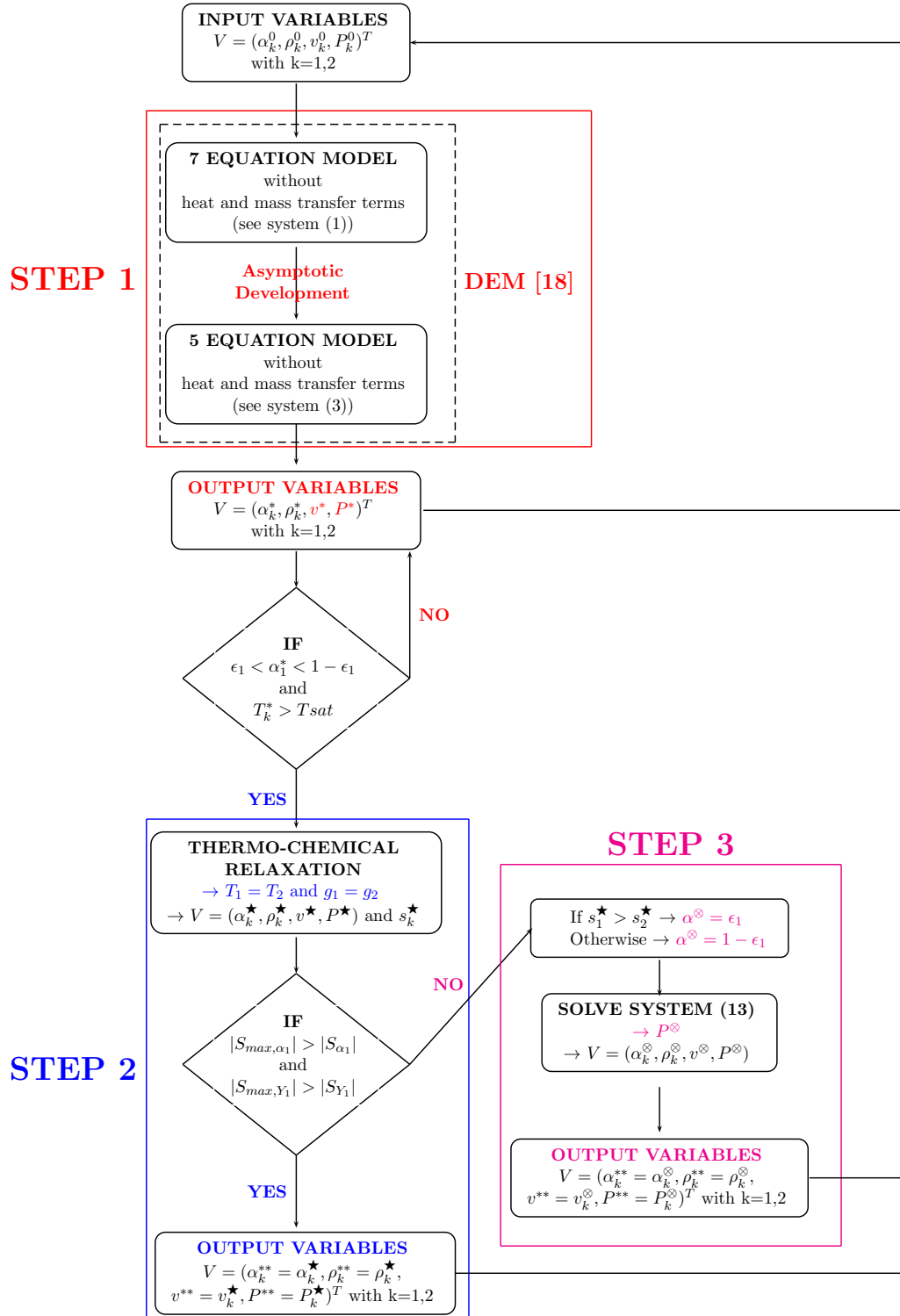


Figure 2: Sketch of the numerical scheme proposed in order to find the numerical solution of system (3).

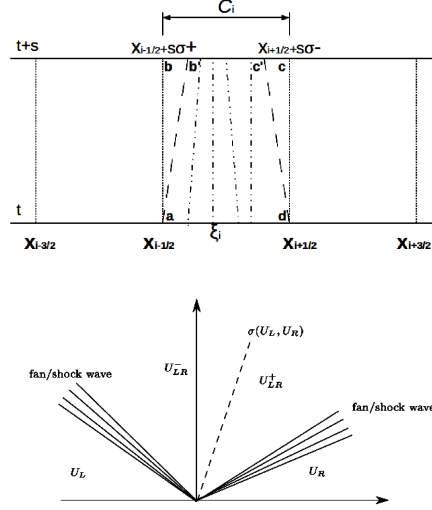


Figure 3: a) Subdivision of the computational domain. b) The various states in the Riemann problem between states U_L and U_R .

In [29], a semi-discrete equation for the discretization of a seven-equation model (see Eq. (1)) has been developed. Then, in [26], an asymptotic development has been applied on the numerical approximation of [29], obtaining the semi-discrete equation for the reduced model (see Eq. (3)). This last one is used in this work and its formulation is the following:

$$\begin{aligned}
\frac{\partial \alpha_1}{\partial t} &= FT_\alpha(U_1) + \frac{\alpha_1 \alpha_2}{\alpha_2 \rho_1 a_1^2 + \alpha_1 \rho_2 a_2^2} \left\{ \frac{FT_\alpha(U_8)}{\alpha_2 \rho_2 \chi_2} - \frac{u_2 FT_\alpha(U_7)}{\alpha_2 \rho_2 \chi_2} + \right. \\
&\quad + \frac{\frac{u_2^2}{2} - e_2 - \rho_2 \kappa_2}{\alpha_2 \rho_2 \chi_2} FT_\alpha(U_6) + \frac{\rho_2^2 \kappa_2 FT_\alpha(U_1)}{\alpha_2 \rho_2 \chi_2} - \frac{FT_\alpha(U_4)}{\alpha_1 \rho_1 \chi_1} + \\
&\quad \left. + \frac{u_1 FT_\alpha(U_3)}{\alpha_1 \rho_1 \chi_1} - \frac{\frac{u_1^2}{2} - e_1 - \rho_1 \kappa_1}{\alpha_1 \rho_1 \chi_1} FT_\alpha(U_2) - \frac{\rho_1^2 \kappa_1 FT_\alpha(U_5)}{\alpha_1 \rho_1 \chi_1} \right\} \\
\frac{\partial \alpha_1 \rho_1}{\partial t} &= FT_{\alpha_1 \rho_1}(U_2) \\
\frac{\partial \alpha_2 \rho_2}{\partial t} &= FT_{\alpha_2 \rho_2}(U_6) \\
\frac{\partial \rho u}{\partial t} &= FT_{\partial \rho u}(U_3) + FT_{\partial \rho u}(U_7) \\
\frac{\partial \rho E}{\partial t} &= FT_{\rho E}(U_4) + FT_{\rho E}(U_8)
\end{aligned} \tag{5}$$

The vector $FT(U_j) = (FT_\alpha, FT_{\alpha_1 \rho_1}, FT_{\alpha_2 \rho_2}, FT_{\rho u}, FT_{\rho E})$, with $j = 1, \dots, 8$, is defined by

$$\begin{aligned}
FT(U_j) &= \frac{1}{\Delta x} \mathcal{E} \left(X(x_{i+1/2}, t) F(U_{i+1/2}^*) - X(x_{i-1/2}, t) F(U_{i-1/2}^*) \right) + \\
&\quad + \frac{1}{\Delta x} \left(\mathcal{E}([X]_{j=0}) F^{lag}(U_i^-, U_{i-1}^+) - \mathcal{E}([X]_{j=N}) F^{lag}(U_i^+, U_{i+1}^-) \right), \tag{6}
\end{aligned}$$

Flow Patterns	Jump indicator	Flux Indicator
$\Sigma_1 - \Sigma_2$	$[X]_{1,1} = 0$	$\left(\beta_{i+1/2}^{(1,2)}\right) = \begin{cases} 1 & \text{if } \sigma(U_i^l, U_{i+1}^r) \geq 0 \\ -1 & \text{if } \sigma(U_i^l, U_{i+1}^r) < 0 \end{cases}$
$\Sigma_1 - \Sigma_1$	$[X]_{1,2} = \begin{cases} -1 & \text{if } \sigma(1, 2) > 0 \\ 0 & \text{otherwise} \end{cases}$	1
$\Sigma_2 - \Sigma_1$	$[X]_{2,1} = \begin{cases} 1 & \text{if } \sigma(2, 1) > 0 \\ 0 & \text{otherwise} \end{cases}$	$\left(\beta_{i+1/2}^{(2,1)}\right) = \begin{cases} 1 & \text{if } \sigma(U_i^l, U_{i+1}^r) \geq 0 \\ -1 & \text{if } \sigma(U_i^l, U_{i+1}^r) < 0 \end{cases}$
$\Sigma_2 - \Sigma_2$	$[X]_{2,2} = 0$	0

Table 1: The various flow configurations at cell boundary $i + 1/2$.

where $U_{i+1/2}^*$ (or $U_{i+1/2}^+$) denotes the solution of Riemann problem between U_i^+ and U_{i+1}^- (respectively, U_{i-1}^+ and U_i^-). The quantities $[X]_{j=0}$ and $[X]_{j=N}$ are the jumps of X at the beginning and at the end of the computational cell, respectively.

Note that the correspondence of the semi-discrete system (5) with the model (3) has been demonstrated in [26]. We notice that this method assumes initially two different thermodynamic states of phases, and at the end of the time step, the states have relaxed to a mechanical equilibrium. On the contrary, a direct discretization of the system (3) assumes directly the equality of initial pressure and velocity of the phases. Following [29, 26], the idea of DEM method is to avoid the introduction of an approximated estimation of fluxes expectancy, $\mathcal{E}(\cdot)$. So, this is estimated from the probability to find in two neighbor cells, the same phase or two different phases (see the "flow patterns" in the Table 1). Then, conservative and non-conservative terms of the system (5) can be developed assuming the four possible types of fluid phase discontinuities.

The terms of the vector $FT(U_j)$ of equation (5) can be computed as follows:

$$\begin{aligned}
 \mathcal{E}\left(X(x_{i+\frac{1}{2}}, t)F(U_{i+\frac{1}{2}}^*)\right) &= \mathcal{P}_{i+\frac{1}{2}}(\Sigma_1, \Sigma_1)F(U_i^{(1)}, U_{i+1}^{(1)}) + \\
 &\quad + \mathcal{P}_{i+\frac{1}{2}}(\Sigma_1, \Sigma_2)\left(\beta_{i+\frac{1}{2}}^{(1,2)}\right)F(U_i^{(1)}, U_{i+1}^{(2)}) \\
 &\quad + \mathcal{P}_{i+\frac{1}{2}}(\Sigma_2, \Sigma_1)\left(\beta_{i+\frac{1}{2}}^{(2,1)}\right)F(U_i^{(2)}, U_{i+1}^{(1)}) \\
 \mathcal{E}\left(X(x_{i-\frac{1}{2}}, t)F(U_{i-\frac{1}{2}}^*)\right) &= \mathcal{P}_{i-\frac{1}{2}}(\Sigma_1, \Sigma_1)F(U_{i-1}^{(1)}, U_i^{(1)}) + \\
 &\quad + \mathcal{P}_{i-\frac{1}{2}}(\Sigma_1, \Sigma_2)\left(\beta_{i-\frac{1}{2}}^{(1,2)}\right)F(U_{i-1}^{(1)}, U_i^{(2)}) \\
 &\quad + \mathcal{P}_{i-\frac{1}{2}}(\Sigma_2, \Sigma_1)\left(\beta_{i-\frac{1}{2}}^{(2,1)}\right)F(U_{i-1}^{(2)}, U_i^{(1)}) \\
 \mathcal{E}\left([X]_N F^{lag}(U_i^{N(w)}, U_{i+1}^-)\right) &= \mathcal{P}_{1+1/2}(\Sigma_1, \Sigma_2)\left(\beta_{i+1/2}^{(1,2)}\right)F^{lag}(U_i^{(1)}, U_{i+1}^{(2)}) \\
 &\quad - \mathcal{P}_{1+1/2}(\Sigma_2, \Sigma_1)\left(\beta_{i+1/2}^{(2,1)}\right)F^{lag}(U_i^{(2)}, U_{i+1}^{(1)}) \\
 \mathcal{E}\left([X]_0 F^{lag}(U_{i-1}^+, U_i^0)\right) &= -\mathcal{P}_{1-1/2}(\Sigma_1, \Sigma_2)\left(\beta_{i-1/2}^{(1,2)}\right)F^{lag}(U_{i-1}^{(1)}, U_i^{(2)}) + \\
 &\quad + \mathcal{P}_{1-1/2}(\Sigma_2, \Sigma_1)\left(\beta_{i-1/2}^{(2,1)}\right)F^{lag}(U_{i-1}^{(2)}, U_i^{(1)})
 \end{aligned}$$

where χ_k and κ_k are defined as follows:

$$\chi_k = \left(\frac{\partial e_k}{\partial P_k}\right)_{\rho_k}, \quad \kappa_k = \left(\frac{\partial e_k}{\partial \rho_k}\right)_{P_k}, \quad (7)$$

e_k is the phase internal energy.

It remains to evaluate the probabilities $\mathcal{P}_{i\pm 1/2}(\Sigma_p, \Sigma_q)$ (see [29]). For simplicity, we only show the final formulation for $i + 1/2$:

$$\begin{aligned} \mathcal{P}_{i+1/2}(\Sigma_1, \Sigma_1) &= \min(\alpha_i^{(1)}, \alpha_{i+1}^{(1)}), & \mathcal{P}_{i+1/2}(\Sigma_2, \Sigma_1) &= \max(\alpha_i^{(2)} - \alpha_{i+1}^{(2)}, 0) \\ \mathcal{P}_{i+1/2}(\Sigma_1, \Sigma_2) &= \min(\alpha_i^{(2)}, \alpha_{i+1}^{(2)}), & \mathcal{P}_{i+1/2}(\Sigma_1, \Sigma_2) &= \max(\alpha_i^{(1)} - \alpha_{i+1}^{(1)}, 0) \end{aligned} \quad (8)$$

where Σ_k indicates the phase, with $k = 1, 2$.

The numerical flux $F(U)$ is approximated via an approximate Riemann solver which can define the contact speed $\sigma(U_L, U_R)$, allowing to define also the Lagrangian flux F^{lag} (see Eq. (4)). In this paper, we have used the relaxation solver [31] for all computations (see [26] for more details). A second order has been applied by means of a predictor-corrector approach that is an extension to a multiphase flows of the MUSCL method shown in [32]. It has been extensively explained in [29]. The time step is constrained by

$$|\lambda_{max}| \frac{\Delta x}{\Delta t} \leq \frac{1}{2}.$$

The semi-discrete equation (5) is solved in order to find the solution of the hyperbolic system with mechanical equilibrium. This strategy allows to start from two completely different thermodynamic states as in the seven-equation models, but finally, to find the mechanical equilibrium solution of a five equation model.

We denote with superscript “0” the initial quantities at time $t=0$ and with superscript \star the quantities computed by solving Step 1. In Table 2, the input and output quantities of the first step are reported. In order to close the system (3), an equation of state (EOS) for each phase and for the mixture is used (see Section 4, and for more details Ref. [14]).

Step 1	
IN variables	OUT variables
α_1^0 ($\alpha_2^0 = 1 - \alpha_1^0$)	α_1^\star ($\alpha_2^\star = 1 - \alpha_1^\star$)
ρ_1^0 and ρ_2^0	ρ_1^\star and ρ_2^\star
v_1^0 and v_2^0	v^\star
P_1^0 and P_2^0	P^\star
e_1^0 and e_2^0	e_1^\star and e_2^\star
T_1^0 and T_2^0	T_1^\star and T_2^\star
g_1^0 and g_2^0	g_1^\star and g_2^\star

Table 2: Variables used in the Step 1.

3.2 Step 2: Numerical solution of the temporal ODEs with heat and mass transfer terms

After considering the hydrodynamic evolution, let us focus now on the numerical treatment of heat and mass transfer terms. The following ODEs equation system

allows to let evolve the solution, considering the new source terms:

$$\begin{aligned}
 \frac{\partial \alpha_1}{\partial t} &= \eta Q + \frac{\rho}{\rho_I} \dot{Y} := S_{\alpha_1} \\
 \frac{\partial \alpha_1 \rho_1}{\partial t} &= \rho \dot{Y} := S_{Y_1} \\
 \frac{\partial \alpha_2 \rho_2}{\partial t} &= -\rho \dot{Y} := -S_{Y_1} \\
 \frac{\partial \rho v}{\partial t} &= 0, & \frac{\partial \rho E}{\partial t} &= 0.
 \end{aligned} \tag{9}$$

where: $Q = \theta(T_2 - T_1)$ and $\dot{Y} = \nu(g_2 - g_1)$. The Gibbs free energy (chemical potential), g_k , are defined for a stiffened gas equation of state, as follows:

$$g_k(P, T_k) = (\gamma_k C v_k - q') T_k - C v_k T_k \log \left(\frac{T_k^{(\gamma_k)}}{(P + P_{\infty, k})^{\gamma_k - 1}} \right).$$

The interface density has been defined in [19] and it has been determined assuming an isentropic behavior of acoustic waves, as follows:

$$\rho_I = \frac{\frac{\rho_1 c_1^2}{\alpha_1} + \frac{\rho_2 c_2^2}{\alpha_2}}{\frac{c_1^2}{\alpha_1} + \frac{c_2^2}{\alpha_2}} \tag{10}$$

Parameters θ and ν are the thermal and chemical relaxation parameters, respectively.

To identify the liquid/vapor interface, the method proposed in [19] and then in [20, 21] is used. In particular, the relaxation parameters θ and ν are set to zero far from the interfaces, and they are taken as infinite in order to fulfill equilibrium interface conditions with mass transfer:

$$\theta, \nu = \begin{cases} +\infty & \text{if } \epsilon \leq \alpha_1 \leq 1 - \epsilon \\ 0 & \text{otherwise,} \end{cases} \tag{11}$$

where ϵ is a very low value. In order to define this value, we first remember that a limit of this model is that a phase can not completely disappear. This means that in all cells, the two phases always coexist. Anyway, a cell is considered filled by a pure fluid, when its volume and mass fraction is equal to $1 - \epsilon_1$, with typically $\epsilon_1 = 10^{-8}$. In other words, in all cells, the gas phase can have a volume fraction value included in $\epsilon_1 < \alpha_g < 1 - \epsilon_1$ and the liquid phase a complementary volume fraction, $\alpha_l = 1 - \alpha_g$, in order to assure that also the other phase exists.

As a consequence, for identifying the interface, $\epsilon = 10^{-6}$ is taken, and the interface corresponds to mixture cells when volume fractions range is between ϵ and $1 - \epsilon$. If ϵ and ϵ_1 are too close, evaporation may occur too early and not only in the interfacial zone.

Moreover, we impose that the mass transfer is allowed only if metastable state is fulfilled, *i.e.* if $T_k > T_{sat}(P^*)$. The saturation temperature has been defined in Section 4.

Let us denote with superscript ‘**’ the final quantities computed by solving Step 1. In Table (3), the input and output quantities of the second step and the

variables that are not influenced by the heat or mass transfer are reported. In fact, from system (11), it is clear that thanks to mass conservation, the mixture density is constant ($\rho^{**} = \rho^*$) and thus, the velocity ($v^{**} = v^*$) and the mixture total and internal energy ($E^{**} = E^*$ and $e^{**} = e^*$).

Remembering that $\alpha_2 = 1 - \alpha_1$, the unknowns of the system (9) are α_1 , ρ_k , v , P , e_k , Q and \dot{Y} . Then, in order to close the system, two ingredients are required : (i) an equation of state for defining the energy as function of pressure and density for both phases (see Section 4) (ii) a thermo-chemical relaxation for finding Q and \dot{Y} . The thermo-chemical relaxation is described in the following sections (Sections 3.2.1 and 3.2.2).

Step 2 (Only at the interface: if $\epsilon_1 < \alpha_1 < 1 - \epsilon_1$ and $T_k > T_{sat}(P^*)$)		
IN variables	OUT variables	Constant MIXTURE variables
α_1^* ($\alpha_2^* = 1 - \alpha_1^*$)	α_1^{**} ($\alpha_2^{**} = 1 - \alpha_1^{**}$)	
ρ_1^* and ρ_2^*	ρ_1^{**} and ρ_2^{**}	
v^*	v^{**}	$\rho^{**} = \rho^*$
P^*	P^{**}	$e^{**} = e^*$
e_1^* and e_2^*	e_1^{**} and e_2^{**}	$E^{**} = E^*$
T_1^* and T_2^*	T^{**}	
g_1^* and g_2^*	g^{**}	

Table 3: Variables used in Step 2. $\rho = (\alpha_1\rho_1) + (\alpha_2\rho_2)$; $\rho e = (\alpha_1\rho_1e_1) + (\alpha_2\rho_2e_2)$; $E = e + \frac{1}{2}v^2$.

3.2.1 Stiff thermo-chemical solver for computing Q and \dot{Y}

It is well-known that, physically, the single phase in metastable state evolves in a new equilibrium liquid/vapor state with a heat and mass exchange. Thus, the mass transfer can stop, only when a new state on the saturation curve is attained, since the liquid and its vapor are in equilibrium. In order to estimate if the two phases are in equilibrium on the saturation curve, it should be assured that, in all time steps, the system achieves the temperature and Gibbs free energy equilibrium between the phases ($T_1 = T_2$ and $g_1 = g_2$).

For solving this issue, a procedure similar to [19] is used. The temperature and the Gibbs time derivatives are computed, that can be written in terms of Q and \dot{Y} , using the mass equations and the energy mixture equation (see Section 3.2.2 for details), as follows:

$$\begin{cases} \frac{\partial \Delta T}{\partial t} = A Q + B \dot{Y} \\ \frac{\partial \Delta g}{\partial t} = A' Q + B' \dot{Y} \end{cases} \quad (12)$$

where A , B , A' and B' should be defined. Assuming that thermodynamic equilibrium is reached at the end of each time step, the simplest numerical approximation of Eq. (12) can be written as follows:

$$\frac{\partial \Delta T}{\partial t} = \frac{\Delta T^{n+1} - \Delta T^n}{\Delta t} = \frac{0 - \Delta T^n}{\Delta t} = A^n Q^n + B^n \dot{Y}^n$$

$$\frac{\partial \Delta g}{\partial t} = \frac{\Delta g^{n+1} - \Delta g^n}{\Delta t} = \frac{0 - \Delta g^n}{\Delta t} = A'^n Q^n + B'^n \dot{Y}^n.$$

Thus, finally, we can determine the heat and mass transfer terms that are computed as follows :

$$\begin{cases} Q = -\frac{B'}{AB' - A'B} \frac{(\Delta T)^n}{\Delta t} + \frac{B}{AB' - A'B} \frac{(\Delta g)^n}{\Delta t} \\ \dot{Y} = \frac{A'}{AB' - A'B} \frac{(\Delta T)^n}{\Delta t} + \frac{A}{AB' - A'B} \frac{(\Delta g)^n}{\Delta t} \end{cases} \quad (13)$$

To compute Q and \dot{Y} , A , B , A' and B' for a five-equation model should be provided. This permits to finalize Step 2. The definitions of these coefficients are provided in the following section.

3.2.2 Definition of A , B , A' and B'

From classical thermodynamical identities, the temporal derivatives of temperature and Gibbs free energy differences can be written as follows :

$$\begin{aligned} \frac{\partial \Delta T}{\partial t} &= \frac{\partial T_2}{\partial t} - \frac{\partial T_1}{\partial t} \\ \frac{\partial \Delta g}{\partial t} &= \frac{\partial(h_2 - T_2 S_2)}{\partial t} - \frac{\partial(h_1 - T_1 S_1)}{\partial t} = \\ &= \frac{1}{\rho_2} \frac{\partial P}{\partial t} - S_2 \frac{\partial T_2}{\partial t} - \frac{1}{\rho_1} \frac{\partial P}{\partial t} + S_1 \frac{\partial T_1}{\partial t} \end{aligned} \quad (14)$$

The temporal derivatives of temperatures and pressure can be defined thanks to mass conservation equations of each phase and to the mixture total energy conservation equation (9). From $\rho_k = \rho(P, T_k)$, the vapor mass conservation equation can be written as :

$$\frac{\partial \alpha_1 \rho_1}{\partial t} = \alpha_1 \frac{\partial \rho_1}{\partial t} + \rho_1 \frac{\partial \alpha_1}{\partial t} = \alpha_1 \left(\left. \frac{\partial \rho_1}{\partial T_1} \right|_P \frac{\partial T_1}{\partial t} + \left. \frac{\partial \rho_1}{\partial P} \right|_{T_1} \frac{\partial P}{\partial t} \right) + \rho_1 \frac{\partial \alpha_1}{\partial t} = \rho \dot{Y} \quad (15)$$

If a stiffened gas equation of state is used (for the equation 29c), it follows that:

$$\left. \frac{\partial \rho_1}{\partial T_1} \right|_P = -\frac{\rho_1}{T_1} \quad \text{and} \quad \left. \frac{\partial \rho_1}{\partial P} \right|_{T_1} = \frac{1}{(\gamma_1 - 1) C v_1 T_1} = \frac{\gamma_1}{c_1^2},$$

where c_k is the phase speed of sound. Thus, after some manipulations, the equation (15) becomes:

$$\boxed{\frac{\partial P}{\partial t} = \frac{c_1^2}{\alpha_1 \gamma_1} \left(\rho \dot{Y} - \rho_1 \frac{\partial \alpha_1}{\partial t} + \frac{\alpha_1 \rho_1}{T_1} \frac{\partial T_1}{\partial t} \right)}. \quad (16)$$

The same procedure can be applied to liquid mass conservation equation of (9), obtaining:

$$-\frac{\alpha_2 \rho_2}{T_2} \frac{\partial T_2}{\partial t} + \frac{\alpha_2 \gamma_2}{c_2^2} \frac{\partial P}{\partial t} - \rho_2 \frac{\partial \alpha_2}{\partial t} = -\rho \dot{Y} \quad (17)$$

Now, using (16) in (17), the partial derivative of liquid temperature can be obtained :

$$\boxed{\frac{\partial T_2}{\partial t} = \frac{T_2}{\alpha_2 \rho_2} \left(\frac{D_2}{D_1} \frac{\alpha_1 \rho_1}{T_1} \frac{\partial T_1}{\partial t} + C_2 \dot{Y} - C_1 \frac{\partial \alpha_1}{\partial t} \right)} \quad (18)$$

where:

$$\begin{aligned} D_1 &= \alpha_1 \gamma_1 c_2^2 \\ D_2 &= \alpha_2 \gamma_2 c_1^2 \\ C_1 &= \frac{D_2 \rho_1 + D_1 \rho_2}{D_1} \\ C_2 &= \left(\frac{D_2 + D_1}{D_1} \right) \rho \end{aligned}$$

Another equation is required to determine the partial derivative of vapor temperature. Remembering that in Step 2 the mixture ρ , ρv and ρE are constant, the following expression can be written:

$$\frac{\partial \rho e}{\partial t} = e_1 \frac{\partial \alpha_1 \rho_1}{\partial t} + e_2 \frac{\partial \alpha_2 \rho_2}{\partial t} + \alpha_1 \rho_1 \frac{\partial e_1}{\partial t} + \alpha_2 \rho_2 \frac{\partial e_2}{\partial t} = 0. \quad (19)$$

Since $(\partial \alpha_1 \rho_1 / \partial t = \rho \dot{Y})$ and $\partial \alpha_2 \rho_2 / \partial t = -\rho \dot{Y}$ and by supposing that $e_k = e(\rho_k, T_k)$, Eq. (19) can be written as:

$$(e_1 - e_2) \rho \dot{Y} + Y_1 \rho \left(\frac{\partial e_1}{\partial T_1} \Big|_{\rho_1} \frac{\partial T_1}{\partial t} + \frac{\partial e_1}{\partial \rho_1} \Big|_{T_1} \frac{\partial \rho_1}{\partial t} \right) + Y_2 \rho \left(\frac{\partial e_2}{\partial T_2} \Big|_{\rho_2} \frac{\partial T_2}{\partial t} + \frac{\partial e_2}{\partial \rho_2} \Big|_{T_2} \frac{\partial \rho_2}{\partial t} \right) = 0, \quad (20)$$

where $Y_k = \alpha_k \rho_k / \rho$. The Eq.29b allows an easy computation of the partial derivatives, as follows:

$$\begin{aligned} \frac{\partial e_k}{\partial T_k} \Big|_{\rho_k} &= C v_k \\ \frac{\partial e_k}{\partial \rho_k} \Big|_{T_k} &= -\frac{P_{\infty, k}}{\rho_k^2}. \end{aligned}$$

Moreover, from the phase mass equations and the vapor volume fraction equation, we can determine $\partial \rho_k / \partial t$ as follows :

$$\begin{aligned} \frac{\partial \rho_1}{\partial t} &= \rho \dot{Y} \left(\frac{1}{\alpha_1} - \frac{\rho_1}{\alpha_1 \rho_I} \right) - \frac{\rho_1}{\alpha_1} \eta Q \\ \frac{\partial \rho_2}{\partial t} &= -\rho \dot{Y} \left(\frac{1}{\alpha_2} - \frac{\rho_2}{\alpha_2 \rho_I} \right) + \frac{\rho_2}{\alpha_2} \eta Q, \end{aligned}$$

where

$$\eta = \frac{\alpha_1 \alpha_2}{\alpha_2 \rho_1 c_1^2 + \alpha_1 \rho_2 c_2^2} \left(\frac{\Gamma_1}{\alpha_1} + \frac{\Gamma_2}{\alpha_2} \right).$$

By replacing all derivatives in Eq. (20), we obtain:

$$\begin{aligned} \left\{ (e_1 - e_2) + \rho \left[\frac{P_{\infty, 2} Y_2}{\rho_2^2} \left(\frac{1}{\alpha_2} - \frac{\rho_2}{\alpha_2 \rho_I} \right) - \frac{P_{\infty, 1} Y_1}{\rho_1^2} \left(\frac{1}{\alpha_1} - \frac{\rho_1}{\alpha_1 \rho_I} \right) \right] \right\} \dot{Y} + \\ + \left[Y_1 \frac{P_{\infty, 1}}{\rho_1 \alpha_1} - Y_2 \frac{P_{\infty, 2}}{\rho_2 \alpha_2} \right] \eta Q + Y_1 C_{v_1} \frac{\partial T_1}{\partial t} + Y_2 C_{v_2} \frac{\partial T_2}{\partial t} = \quad (21) \\ = \theta_1 \dot{Y} + Z_1 \eta Q + Y_1 C_{v_1} \frac{\partial T_1}{\partial t} + Y_2 C_{v_2} \frac{\partial T_2}{\partial t} = 0, \quad \text{Inria} \end{aligned}$$

where

$$\theta_1 = (e_1 - e_2) + \rho \left[\frac{P_{\infty,2} Y_2}{\rho_2^2} \left(\frac{1}{\alpha_2} - \frac{\rho_2}{\alpha_2 \rho_I} \right) - \frac{P_{\infty,1} Y_1}{\rho_1^2} \left(\frac{1}{\alpha_1} - \frac{\rho_1}{\alpha_1 \rho_I} \right) \right]$$

and

$$Z_1 = Y_1 \frac{P_{\infty,1}}{\rho_1 \alpha_1} - Y_2 \frac{P_{\infty,2}}{\rho_2 \alpha_2}.$$

We can replace, now, the partial derivative of liquid temperature T_2 (see Eq. 18):

$$\frac{\partial T_1}{\partial t} = \frac{T_1 D_1}{Y_1 (C_{v1} T_1 D_1 + C_{v2} T_2 D_2)} \left\{ -\dot{Y} \left[\theta_1 + \frac{T_2 C_{v2}}{\rho} \left(C_2 - \frac{\rho}{\rho_I} \right) \right] - Q \eta \left(Z_1 - \frac{T_2 C_{v2}}{\rho} C_1 \right) \right\}. \quad (22)$$

Let us consider the system composed by the equations (16), (18) and (22):

$$\begin{aligned} \frac{\partial P}{\partial t} &= \frac{c_1^2}{\alpha_1 \gamma_1} \left(\rho \dot{Y} - \rho_1 \frac{\partial \alpha_1}{\partial t} + \frac{\alpha_1 \rho_1}{T_1} \frac{\partial T_1}{\partial t} \right) \\ \frac{\partial T_2}{\partial t} &= \frac{T_2}{\alpha_2 \rho_2} \left(\frac{D_2}{D_1} \frac{\alpha_1 \rho_1}{T_1} \frac{\partial T_1}{\partial t} + C_2 \dot{Y} - C_1 \frac{\partial \alpha_1}{\partial t} \right) \\ \frac{\partial T_1}{\partial t} &= \frac{T_1 D_1}{Y_1 (C_{v1} T_1 D_1 + C_{v2} T_2 D_2)} \left\{ -\dot{Y} \left[\theta_1 + \frac{T_2 C_{v2}}{\rho} \left(C_2 - \frac{\rho}{\rho_I} \right) \right] - Q \eta \left(Z_1 - \frac{T_2 C_{v2}}{\rho} C_1 \right) \right\}. \end{aligned} \quad (23)$$

By replacing the temporal derivative of the vapor volume fraction ($\frac{\partial \alpha_1}{\partial t} = \eta Q + \frac{\rho}{\rho_I} \dot{Y}$), the temporal derivatives of the phase temperatures and pressure can be obtained as a function of \dot{Y} and Q :

$$\begin{aligned} \frac{\partial T_1}{\partial t} &= \xi \left\{ -\dot{Y} \left[\theta_1 + \frac{T_2 C_{v2}}{\rho} \left(C_2 - \frac{\rho}{\rho_I} \right) \right] - Q \eta \left(Z_1 - \frac{T_2 C_{v2}}{\rho} C_1 \right) \right\} \\ \frac{\partial T_2}{\partial t} &= \frac{T_2 D_2 Y_1}{T_1 D_1 Y_2} \frac{\partial T_1}{\partial t} + \frac{T_2}{\alpha_2 \rho_2} \left[\dot{Y} \left(C_2 - C_1 \frac{\rho}{\rho_I} \right) - C_1 \eta Q \right] \\ \frac{\partial P}{\partial t} &= \frac{c_1^2 \rho_1}{\gamma_1 T_1} \frac{\partial T_1}{\partial t} + \frac{c_1^2}{\alpha_1 \gamma_1} \left[\dot{Y} \left(\rho - \rho_1 \frac{\rho}{\rho_I} \right) - \rho_1 \eta Q \right], \end{aligned} \quad (24)$$

where $\xi = \frac{T_1 D_1}{Y_1(C_{v_1} T_1 D_1 + C_{v_2} T_2 D_2)}$. Finally, substituting (24) in (14), it follows:

$$\begin{aligned}
AQ + B\dot{Y} &= -Q \left[\xi \left(\frac{T_2 D_2 Y_1}{T_1 D_1 Y_2} - 1 \right) \left(Z_1 \eta - \frac{T_2 C_{v_2}}{\rho} C_1 \eta \right) + \frac{T_2}{\alpha_2 \rho_2} C_1 \eta \right] + \\
&\quad + \dot{Y} \left[-\xi \left(\frac{T_2 D_2 Y_1}{T_1 D_1 Y_2} - 1 \right) \left(\theta_1 + \frac{T_2 C_{v_2}}{\rho} \left(C_2 - \frac{\rho}{\rho_I} \right) \right) + \frac{T_2}{\alpha_2 \rho_2} \left(C_2 - C_1 \frac{\rho}{\rho_I} \right) \right], \\
A'Q + B'\dot{Y} &= Q \left[-\left(\frac{1}{\rho_2} - \frac{1}{\rho_1} \right) \frac{c_1^2}{\alpha_1 \gamma_1} \rho_1 \eta + \frac{S_2 T_2}{\alpha_2 \rho_2} C_1 \eta - \xi \delta_1 \left(Z_1 \eta - \frac{T_2 C_{v_2}}{\rho} C_1 \eta \right) \right] \\
&\quad + \dot{Y} \left\{ \left(\frac{1}{\rho_2} - \frac{1}{\rho_1} \right) \frac{c_1^2}{\alpha_1 \gamma_1} \left(\rho - \rho_1 \frac{\rho}{\rho_I} \right) - \frac{S_2 T_2}{\alpha_2 \rho_2} \left(C_2 - C_1 \frac{\rho}{\rho_I} \right) \right. \\
&\quad \quad \left. - \xi \delta_1 \left[\theta_1 + \frac{T_2 C_{v_2}}{\rho} \left(C_2 - \frac{\rho}{\rho_I} \right) \right] \right\}, \tag{25}
\end{aligned}$$

where

$$\delta_1 = \left(\frac{1}{\rho_2} - \frac{1}{\rho_1} \right) \frac{c_1^2 \rho_1}{T_1 \gamma_1} + S_1 - S_2 \frac{T_2 D_2 Y_1}{T_1 D_1 Y_2}.$$

Considering the system (25), we can define the coefficients A , B , A' , B' as follows:

$$\begin{aligned}
A &= -\xi \left[\left(\frac{T_2 D_2 Y_1}{T_1 D_1 Y_2} - 1 \right) \left(Z_1 \eta - \frac{T_2 C_{v_2}}{\rho} C_1 \eta \right) + \frac{T_2}{\alpha_2 \rho_2} C_1 \eta \right] \\
B &= -\xi \left(\frac{T_2 D_2 Y_1}{T_1 D_1 Y_2} - 1 \right) \left[\theta_1 + \frac{T_2 C_{v_2}}{\rho} \left(C_2 - \frac{\rho}{\rho_I} \right) \right] + \frac{T_2}{\alpha_2 \rho_2} \left(C_2 - C_1 \frac{\rho}{\rho_I} \right) \\
A' &= -\left(\frac{1}{\rho_2} - \frac{1}{\rho_1} \right) \frac{c_1^2}{\alpha_1 \gamma_1} \rho_1 \eta + \frac{S_2 T_2}{\alpha_2 \rho_2} C_1 \eta - \xi \delta_1 \left(Z_1 \eta - \frac{T_2 C_{v_2}}{\rho} C_1 \eta \right) \\
B' &= \left(\frac{1}{\rho_2} - \frac{1}{\rho_1} \right) \frac{c_1^2}{\alpha_1 \gamma_1} \left(\rho - \rho_1 \frac{\rho}{\rho_I} \right) - \frac{S_2 T_2}{\alpha_2 \rho_2} \left(C_2 - C_1 \frac{\rho}{\rho_I} \right) + \\
&\quad - \xi \delta_1 \left[\theta_1 + \frac{T_2 C_{v_2}}{\rho} \left(C_2 - \frac{\rho}{\rho_I} \right) \right] \tag{26}
\end{aligned}$$

3.3 Step 3: Mass fraction and density positivity

The approximation of heat and mass transfer terms allow the calculation of source terms of volume fraction and mass conservative equations, but there is no guarantee that positivity of the solution be preserved. Assuming an evaporation process for example, the mass source terms estimated can be larger than the liquid mass fraction that can evaporate. So, as in [19], a limitation is placed on the source terms, by determining the maximum admissible values, as follows:

$$S_{max, \alpha_1} = \begin{cases} \frac{1-\alpha_1}{\Delta t} & \text{if } S_{max} > 0 \\ \frac{-\alpha_1}{\Delta t} & \text{otherwise,} \end{cases} \quad S_{max, Y_1} = \begin{cases} \frac{(1-\alpha_1)\rho_2}{\Delta t} & \text{if } S_{max} > 0 \\ \frac{-\alpha_1 \rho_1}{\Delta t} & \text{otherwise.} \end{cases}$$

Thus, if $|S_{max,\alpha_1}| > |S_{\alpha_1}|$ and $|S_{max,Y_1}| > |S_{Y_1}|$, the source terms is used.

Otherwise, if the limit value is not respected, a new method is introduced in order to avoid an integration of the system over a fractional hydrodynamic time step, as it is done in [19, 20]. We assumed that the mixture is composed nearly of the species k that has the highest entropy, using an idea similar to [21, 33]. In particular, let us indicate with \star the variable value at the end of positivity system check control:

- if $s_g^\star > s_l^\star$, then the vapor volume fraction, α^{**} , is fixed to $1 - \epsilon_1$,
- otherwise, if $s_g^\star < s_l^\star$, then α^{**} is fixed to ϵ_1 ,

where, as explained in Section 3.2, $\epsilon_1 = 10^{-8}$.

Knowing α^{**} , it can be used in the following system in order to find the new equilibrium pressure, P^{**} , and temperature, T^{**} , and, then the other thermodynamic variables (a stiffened equation of state is assumed) :

$$\begin{aligned}\rho^{**} &= (\alpha_1 \rho_1)^{**} + (\alpha_2 \rho_2)^{**} = \rho^\star \\ (\rho e)^{**} &= (\alpha_1 \rho_1 e_1)^{**} + (\alpha_2 \rho_2 e_2)^{**} = (\rho e)^\star \\ \rho_k^{**}(P^{**}, T^{**}) &= \frac{P^{**} + P_{\infty,k}}{C_{v_k} \Gamma_k T^{**}} \\ (\rho e)_k^{**}(P^{**}, T^{**}) &= \frac{P^{**} + P_{\infty,k} \gamma_k}{\Gamma_k} + \rho_k^{**} q\end{aligned}\quad (27)$$

where $\Gamma = \gamma - 1$. By replacing the phase density, ρ_k^{**} , and the phase energy $(\rho e)_k^{**}$, in the first two equations of system (27), we obtain a single quadratic equation for P^{**} :

$$\begin{aligned}T^{**} &= \frac{\alpha_1^{**} C_{v_2} \Gamma_2 (P^{**} + P_{\infty,1}) + \alpha_2^{**} C_{v_1} \Gamma_1 (P^{**} + P_{\infty,2})}{\rho^\star C_{v_1} \Gamma_1 C_{v_2} \Gamma_2} \\ 0 &= (P^{**})^2 + b P^{**} + d\end{aligned}\quad (28)$$

and:

$$\begin{aligned}b &= \frac{F_1}{F_2} + \frac{q_1(\alpha_1^{**} C_{v_2} \Gamma_2) + q_2(\alpha_2^{**} C_{v_1} \Gamma_1)}{Z_2} + F_2 \frac{P_{\infty,1}(\alpha_1^{**} C_{v_2} \Gamma_2) + P_{\infty,2}(\alpha_2^{**} C_{v_1} \Gamma_1)}{\rho^\star \Gamma_1 \Gamma_2} \\ d &= \frac{F_1}{Z_2} \frac{P_{\infty,1}(\alpha_1^{**} C_{v_2} \Gamma_2) + P_{\infty,2}(\alpha_2^{**} C_{v_1} \Gamma_1)}{\rho^\star \Gamma_1 \Gamma_2} + \frac{P_{\infty,1} q_1(\alpha_1^{**} C_{v_2} \Gamma_2) + P_{\infty,2} q_2(\alpha_2^{**} C_{v_1} \Gamma_1)}{Z_2}\end{aligned}$$

where

$$\begin{aligned}F_1 &= P_{\infty,1} \gamma_1 \frac{(\alpha_1^{**} C_{v_2} \Gamma_2)}{C_{v_2}} + P_{\infty,2} \gamma_2 \frac{(\alpha_2^{**} C_{v_1} \Gamma_1)}{C_{v_1}} - (\rho e)^\star \Gamma_1 \Gamma_2 \\ F_2 &= \alpha_1^{**} \Gamma_2 + \alpha_2^{**} \Gamma_1 \\ Z_2 &= F_2 \frac{(\alpha_1^{**} C_{v_2} \Gamma_2) + (\alpha_2^{**} C_{v_1} \Gamma_1)}{\rho^{**} \Gamma_1 \Gamma_2}.\end{aligned}$$

Then, by solving the single quadratic equation of P^{**} , we select the physically admissible solution of the quadratic equation that maximizes the total entropy $s^{**} = Y_1^{**} s_1^{**} + Y_2^{**} s_2^{**}$, where $Y_k^{**} = (\alpha_k^{**} \rho_k^{**}) / \rho^{**}$

This procedure allows to reduce the computational cost compared to [19, 20]: it is not necessary to integrate over a fractional hydrodynamic time step.

4 Thermodynamic closure

As we have previously mentioned, we deal with pure fluid and artificial mixture zone, thus the EOS must be able to describe flows both in pure fluids and mixture zones.

In order to clarify this point, let us remember that, in the system (3), the last two equations are the momentum and energy conservation equations for the mixture, in which, a mixture pressure P appears. For this reason, a mixture EOS for extrapolating the value of P , is required.

4.1 Stiffened Gas EOS for pure fluid

The Stiffened Gas EOS is usually used for shock dynamics and its robustness for simulating two-phase flow with or without mass transfer has been amply demonstrated (see for example [29, 15, 34, 26, 35]). It can be written as follows:

$$P(\rho, e) = (\gamma - 1)(e - q)\rho - \gamma P_\infty, \quad (29a)$$

$$e(\rho, T) = Tc_v + \frac{P_\infty}{\rho} + q \quad (29b)$$

$$\rho(P, T) = \frac{P + P_\infty}{(\gamma - 1)c_v T} \quad (29c)$$

$$h(T) = \gamma c_v T, \quad (29d)$$

$$s(P, T) = c_v \ln \frac{T^\gamma}{(P + P_\infty)^{(\gamma-1)}} + q', \quad (29e)$$

$$g(P, T) = h(T) - Ts(P, T), \quad (29f)$$

where P , ρ and e are the pressure, the density and the energy, respectively. The polytropic coefficient γ is the constant ratio of specific heat capacities $\gamma = c_p/c_v$, P_∞ is a constant reference pressure and q is the energy of the fluid at a given reference state. Moreover, T , c_v and h are the temperature, the specific heat at constant volume and the enthalpy, respectively. The speed of sound, defined as $c^2 = (\frac{\partial P}{\partial \rho})_s$ can be computed as follows:

$$c^2 = \gamma \frac{P + P_\infty}{\rho} = (\gamma - 1)c_p T \quad (30)$$

where c^2 remains strictly positive (for $\gamma > 1$). It ensures the hyperbolicity of the system and the existence of a convex mathematical entropy [36].

4.2 SG EOS based mixture

The EOS for the mixture can be easily obtained using the EOS of the single phase. The aim is now to obtain the mixture pressure. The starting point is the mixture energy equation:

$$\rho e = \alpha_1 \rho_1 e_1 + \alpha_2 \rho_2 e_2. \quad (31)$$

The energy of each phase, $e_k = \frac{P+P_\infty\gamma}{\rho_k(\gamma_k-1)}$, can be replaced obtaining the mixture total energy as a function of the phase pressures. Under pressure equilibrium, the following expression for the pressure mixture can be obtained:

$$P(\rho, e, \alpha_k) = \frac{\rho(e - \frac{\alpha_1 \rho_1 q_1}{\rho} - \frac{\alpha_2 \rho_2 q_2}{\rho}) - \left(\frac{\alpha_1 \gamma_1 P_{\infty,1}}{\gamma_1 - 1} + \frac{\alpha_2 \gamma_2 P_{\infty,2}}{\gamma_2 - 1} \right)}{\frac{\alpha_1}{\gamma_1 - 1} + \frac{\alpha_2}{\gamma_2 - 1}} \quad (32)$$

4.3 Definition of χ_k and κ_k

For the SG EOS, it is trivial to compute the coefficients of the semi-discrete equation (5) as follows:

$$\chi_k = \left(\frac{\partial e_k}{\partial P_k} \right)_{\rho_k} = \frac{1}{(\gamma - 1)\rho}, \quad (33)$$

$$\kappa_k = \left(\frac{\partial e_k}{\partial \rho_k} \right)_{P_k} = -\frac{P + \gamma P_\infty}{(\gamma - 1)\rho^2}. \quad (34)$$

5 Extension to six and seven-equation model

In this section, the cavitation model is extended to more complex systems of equations. Some hypothesis used in the previous sections are no more valid. In particular, the attention is focused on six (single velocity) and seven-equation models, respectively. Note that step 1 consists always in finding the solution for the hyperbolic part of the model, *i.e.* without the heat and mass transfer terms. As a consequence, a different model is associated to a different discretization of the hyperbolic part. We see that step 1 remains unchanged, contrarily to steps 2 and 3.

5.1 Modeling cavitation with the seven-equation model

For clearly explaining the natural extension of the model proposed in the previous section to the seven-equation model, let us define the different steps, as follows.

5.1.1 Step 1 for a seven-equation model

Let us suppose here that each phase has its own pressure and velocity (see see system (1)). However, during the mass transfer, the two phases have the same pressure, that is equal to the saturation pressure. So, a relaxation procedure should be applied in order to obtain a single pressure system as in [27, 21].

We have assumed that the pressure relaxation is faster than the temperature and the Gibbs free energy relaxation: Step 1 is necessary to find the solution of the system (1) without the heat and mass transfer terms and to apply a pressure relaxation procedure. In this way, variables summarized in Table 4 are obtained.

Step 1 for a seven-equation model	
IN	OUT
α_1^0 ($\alpha_2^0 = 1 - \alpha_1^0$)	α_1^* ($\alpha_2^* = 1 - \alpha_1^*$)
ρ_1^0 and ρ_2^0	ρ_1^* and ρ_2^*
v_1^0 and v_2^0	v_1^* and v_2^*
P_1^0 and P_2^0	P^*
e_1^0 and e_2^0	e_1^* and e_2^*
T_1^0 and T_2^0	T_1^* and T_2^*
g_1^0 and g_2^0	g_1^* and g_2^*

Table 4: Variables used in Step 1 for a seven-equation model

5.1.2 Step 2 for a seven-equation model

As in the five-equation model, if the system is in metastable conditions, *i.e.* ($T_k > T_{sat}$) and at the interface $\epsilon_1 < \alpha_1 < 1 - \epsilon_1$, the ODE system for the seven-equation model (see system (1)) is as follows:

$$\begin{aligned}
\frac{\partial \alpha_1}{\partial t} &= \frac{\alpha_1 \alpha_2}{\alpha_2 \rho_1 c_1^2 + \alpha_1 \rho_2 c_2^2} \left(\frac{\Gamma_1}{\alpha_1} + \frac{\Gamma_2}{\alpha_2} \right) Q + \frac{\rho}{\rho_I} \dot{Y} \\
\frac{\partial(\alpha_1 \rho_1)}{\partial t} &= \rho \dot{Y} \\
\frac{\partial(\alpha_1 \rho_1 v_1)}{\partial t} &= v_I \rho \dot{Y} \\
\frac{\partial(\alpha_1 \rho_1 E_1)}{\partial t} &= Q + E_I \rho \dot{Y} \\
\frac{\partial(\alpha_2 \rho_2)}{\partial t} &= -\rho \dot{Y} \\
\frac{\partial(\alpha_2 \rho_2 v_2)}{\partial t} &= -v_I \rho \dot{Y} \\
\frac{\partial(\alpha_2 \rho_2 E_2)}{\partial t} &= -Q - E_I \rho \dot{Y}.
\end{aligned} \tag{35}$$

Several definitions of the interface pressure, P_I , and velocity, v_I , exist in the literature [29, 37]. For example, in [12], v_I is assumed equal to liquid velocity, v_2 , and P_I equal to vapor pressure, P_1 . Otherwise, more complex definitions can be used, as in [38]:

$$\begin{cases} P_I = \frac{Z_1 P_2 + Z_2 P_1}{Z_1 + Z_2} + \text{sign} \left(\frac{\partial \alpha_1}{\partial x} \right) \frac{(u_2 - u_1)}{Z_1 + Z_2} \\ u_I = \frac{Z_1 u_1 + Z_2 u_2}{Z_1 + Z_2} + \text{sign} \left(\frac{\partial \alpha_1}{\partial x} \right) \frac{P_2 - P_1}{Z_1 + Z_2} \end{cases} \tag{36}$$

where $Z = \rho c$ represents the acoustic impedance and c is the speed of sound.

The variable ρ_I is the interface density and it is defined by means of the equation (10). Remembering that $\alpha_2 = 1 - \alpha_1$, the unknowns of the system (35) are α_1 , ρ_k , v_k , P , e_k , Q , \dot{Y} , E_I . Then, to close the system, the equation of state for defining the energy as function of pressure and density is used for both phases. The interface energy, E_I , will be developed in section 5.1.4. Moreover,

a thermo-chemical relaxation for finding Q and \dot{Y} is imposed, as follows:

$$\begin{aligned}\frac{\partial \Delta T}{\partial t} &= A Q + B \dot{Y} \\ \frac{\partial \Delta g}{\partial t} &= A' Q + B' \dot{Y}.\end{aligned}\quad (37)$$

The procedure described in Section 3.2.2 can be applied in this case without problem, *i.e.* the mass conservation equations and the mixture internal energy ones can be used in order to find the value of the four coefficients A , B , A' and B' . However, the only mixture variable that remains constant from the step 1 to the step 2 is ρ (see Table (5)). This means that, as in Section 3.2.2, the development of equations (15) and (17) do not change and equations (16) and (18) can be obtained. Note also that Eq. (19) is not valid anymore. Then, remembering that, for a seven-equation model,

$$\alpha_1 \rho_1 \frac{\partial u_1}{\partial t} = \rho \dot{Y} (u_I - u_1) \quad (38)$$

and

$$\alpha_2 \rho_2 \frac{\partial u_2}{\partial t} = \rho \dot{Y} (u_I - u_2), \quad (39)$$

the mixture energy equation can be written as follows:

$$\begin{aligned}\frac{\partial \rho e}{\partial t} &= \frac{\partial (\alpha_1 \rho_1 E_1 + \alpha_2 \rho_2 E_2)}{\partial t} - \frac{\partial [\alpha_1 \rho_1 (\frac{1}{2} u_1^2) + \alpha_2 \rho_2 (\frac{1}{2} u_2^2)]}{\partial t} = \\ &= -\frac{1}{2} \rho \dot{Y} (u_2^2 - 2u_2 u_I + 2u_1 u_I - u_1^2) = -\beta \dot{Y}.\end{aligned}\quad (40)$$

By coupling the equation (20) and its developments (until the equation (22)) with the equation (40), this last one can be written as follows:

$$\frac{\partial \rho e}{\partial t} = \theta_1 \dot{Y} + Z_1 \eta Q + Y_1 C_{v_1} \frac{\partial T_1}{\partial t} + Y_2 C_{v_2} \frac{\partial T_2}{\partial t} = -\beta \dot{Y}. \quad (41)$$

As a consequence, by coupling equations (41), (16) and (18), the following new values for the coefficients A , B , A' and B' for the seven-equation model can be obtained:

$$\begin{aligned}A &= - \left[\xi \left(\frac{T_2 D_2 Y_1}{T_1 D_1 Y_2} - 1 \right) \left(Z_1 \eta - \frac{T_2 C_{v_2}}{\rho} C_1 \eta \right) + \frac{T_2}{\alpha_2 \rho_2} C_1 \eta \right] \\ B &= -\xi \left(\frac{T_2 D_2 Y_1}{T_1 D_1 Y_2} - 1 \right) \left[\theta_1 + \frac{T_2 C_{v_2}}{\rho} \left(C_2 - \frac{\rho}{\rho_I} + \beta \right) \right] + \frac{T_2}{\alpha_2 \rho_2} \left(C_2 - C_1 \frac{\rho}{\rho_I} \right) \\ A' &= - \left(\frac{1}{\rho_2} - \frac{1}{\rho_1} \right) \frac{c_1^2}{\alpha_1 \gamma_1} \rho_1 \eta + \frac{S_2 T_2}{\alpha_2 \rho_2} C_1 \eta - \xi \delta_1 \left(Z_1 \eta - \frac{T_2 C_{v_2}}{\rho} C_1 \eta \right) \\ B' &= \left(\frac{1}{\rho_2} - \frac{1}{\rho_1} \right) \frac{c_1^2}{\alpha_1 \gamma_1} \left(\rho - \rho_1 \frac{\rho}{\rho_I} \right) - \frac{S_2 T_2}{\alpha_2 \rho_2} \left(C_2 - C_1 \frac{\rho}{\rho_I} \right) + \\ &\quad - \xi \delta_1 \left[\theta_1 + \frac{T_2 C_{v_2}}{\rho} \left(C_2 - \frac{\rho}{\rho_I} + \beta \right) \right].\end{aligned}$$

Remark that coefficients A and A' are equal to the coefficients of Section 3.2.2. Instead, coefficients B and B' are different only for the term β .

Step 2 for the seven-equation model		
(Only on the interface, if $\epsilon_1 < \alpha_1 < 1 - \epsilon_1$ and $T_k > T_{sat}(P^*)$)		
IN	OUT	Constant mixture variables
α_1^* ($\alpha_2^* = 1 - \alpha_1^*$)	α_1^{**} ($\alpha_2^{**} = 1 - \alpha_1^{**}$)	$\rho^{**} = \rho^*$
ρ_1^* and ρ_2^*	ρ_1^{**} and ρ_2^{**}	
v^*	v_1^{**} and v_2^{**}	
P^*	P^{**}	
e_1^* and e_2^*	e_1^{**} and e_2^{**}	
T_1^* and T_2^*	T^{**}	
g_1^* and g_2^*	g^{**}	

Table 5: Variables used in Step 2 for a seven-equation model. $\rho = (\alpha_1\rho_1) + (\alpha_2\rho_2)$; $\rho e = (\alpha_1\rho_1e_1) + (\alpha_2\rho_2e_2)$; $E = e + \frac{1}{2}v^2$.

5.1.3 Step 3 for a seven-equation model

For the seven-equation model, Step 3 is equal to the one described in Section 3.3, without other modifications.

5.1.4 Determination of E_I

Let us now focus the attention on the definition of the variable E_I (see system of equations 35). Let us start the demonstration from the gas total energy relation:

$$\frac{\partial(\alpha_1\rho_1E_1)}{\partial t} = \alpha_1\rho_1 \frac{\partial(e_1 + \frac{1}{2}u_1^2)}{\partial t} + E_1\rho\dot{Y} = Q + E_I\rho\dot{Y}. \quad (42)$$

By substituting equation (38) in the equation (42), this last one becomes:

$$\alpha_1\rho_1 \frac{\partial e_1}{\partial t} + u_1(u_I - u_1)\rho\dot{Y} + E_1\rho\dot{Y} = Q + E_I\rho\dot{Y}. \quad (43)$$

The energy can be written as a function of density and temperature, $e_1(T_1, \rho_1)$, so the temporal derivative can be written as follows:

$$\begin{aligned} \frac{\partial e_1}{\partial t}(T_1, \rho_1) &= \frac{\partial e_1}{\partial T_1} \Big|_{\rho_1} \frac{\partial T_1}{\partial t} + \frac{\partial e_1}{\partial \rho_1} \Big|_{T_1} \frac{\partial \rho_1}{\partial t} = \\ &= c_{v,1}\xi \left\{ -\dot{Y} \left[\theta_1 + \frac{T_2 C v_2}{\rho} \left(C_2 - \frac{\rho}{\rho_I} + \beta \right) \right] + \right. \\ &\quad \left. - Q \left(Z_1 \eta - \frac{T_2 C v_2}{\rho} C_1 \eta \right) \right\}. \end{aligned} \quad (44)$$

Then, by replacing the equation (45) into the equation (43), after some manipulations, the interface energy can be defined as follows:

$$\begin{aligned} E_I &= -\alpha_1\rho_1 c_{v,1} \frac{\xi}{\rho} \left[\theta_1 + \frac{T_2 C v_2}{\rho} \left(C_2 - \frac{\rho}{\rho_I} + \beta \right) \right] + \\ &\quad + P_{\infty,1} \left(\frac{1}{\rho_I} - \frac{1}{\rho_1} \right) \left(u_1 u_I - \frac{1}{2} u_1^2 + e_1 \right) + \\ &\quad + \frac{Q}{\rho\dot{Y}} \left[P_{\infty,1} \eta - \alpha_1\rho_1 c_{v,1} \xi \left(Z_1 \eta - \frac{T_2 C v_2}{\rho} C_1 \eta \right) - 1 \right]. \end{aligned} \quad (45)$$

5.2 Modeling cavitation for a six-equation model

The six-equation model is based on the assumption that the phase velocities are equal. This can be represented by the following system of equations:

$$\begin{aligned}
\frac{\partial \alpha_1}{\partial t} + v_I \frac{\partial \alpha_1}{\partial x} &= \mu(P_1 - P_2) + \eta Q + \frac{\rho}{\rho_I} \dot{Y} \\
\frac{\partial(\alpha_1 \rho_1)}{\partial t} + \frac{\partial(\alpha_1 \rho_1 v_1)}{\partial x} &= \rho \dot{Y} \\
\frac{\partial(\alpha_2 \rho_2)}{\partial t} + \frac{\partial(\alpha_2 \rho_2 v_2)}{\partial x} &= -\rho \dot{Y} \\
\frac{\partial(\rho v)}{\partial t} + \frac{\partial(\rho v^2 + \alpha_1 P_1 + \alpha_2 P_2)}{\partial x} &= 0 \\
\frac{\partial(\alpha_1 \rho_1 E_1)}{\partial t} + \frac{\partial(\alpha_1(\rho_1 E_1 + P_1)v_1)}{\partial x} &= P_I v_I \frac{\partial \alpha_1}{\partial x} + \lambda v_I (v_2 - v_1) + \\
&\quad + \mu P_I (P_1 - P_2) + Q + E_I \rho \dot{Y} \\
\frac{\partial(\alpha_2 \rho_2 E_2)}{\partial t} + \frac{\partial(\alpha_2(\rho_2 E_2 + P_2)v_2)}{\partial x} &= P_I v_I \frac{\partial \alpha_2}{\partial x} - \lambda v_I (v_2 - v_1) + \\
&\quad - \mu P_I (P_1 - P_2) - Q - E_I \rho \dot{Y}.
\end{aligned} \tag{46}$$

In this case also, it is assumed that, during the mass transfer, the two phases have the same pressure, equal to the saturation pressure. So, a relaxation procedure should be applied in order to obtain a single pressure system as in [21, 20]. This means, that, close to the interface, it is equivalent to a five equation model. As a consequence, all the considerations developed in Section 3.2, and coefficients A , B , A' and B' found in Section 3.2.2, can be equally used for a six-equation model.

6 Results

All the numerical simulations presented in this paper are performed by means of a five equation model coupled with the cavitation model of section 3.2.2. Several numerical test-case are performed. Then, the robustness of the numerical method is assessed on some of the most used numerical configuration in the literature for estimating efficiency of two-phase compressible models. In particular, the aim is to i) show the influence of heat and mass transfer, ii) validate the results by comparison with respect to the experimental data and to the existing state-of-art in terms of numerical simulation, iii) estimate the prediction in terms of important quantities from a physical point of view.

All the numerical test-cases are performed by using liquid and vapor of dodecane or of water. Physical parameters for each test-case are summarized in Table 6. A second order has been performed for all the numerical test-cases by means a Muscl scheme (see [29] for more details), coupled with a Relaxation solver ([31, 26]) and a Minmod limiter. Note also that a mesh-convergence study has been done for each test-case, even if it is not reported here for brevity. The first test case is a classical two phase shock-tube that allows to observe the appearance of the evaporation wave and is a classical test-case in literature. Secondly, the experiment of Simoes-Moreira [39] is reproduced. It reproduces an experimental two phase shock-tube that allows to validate the cavitation model

with respect to the experimental data. The last two test cases are associated to a two-phase expansion tube with different initial phase velocities, which is widely used in literature [21]. These test cases allow to observe the appearance of the evaporation wave in a mixture and not in a pure liquid as in the case of a shock-tube problem.

TEST CASE	FLUID	SG EOS					
		γ	$P_\infty [Pa]$	$C_p [\frac{J}{KgK}]$	$C_v [\frac{J}{KgK}]$	q	q'
1 Shock tube	Liq. Dodecane	2.35	4×10^8	2534	1077	-755×10^3	0
	Vap. Dodecane	1.025	0	2005	1956	-237×10^3	-24.2×10^3
2 Shock tube experiments	Liq. Dodecane	2.35	4×10^8	2534	1077	-755×10^3	0
	Vap. Dodecane	1.025	0	2005	1956	-237×10^3	-24.2×10^3
3-4 Expansion tube	Liq. Water	2.35	10^9	4267	1816	-1167×10^3	0
	Vap. Water	1.43	0	1487	1040	2030×10^3	-23×10^3

Table 6: EOS coefficients for liquid and gas phases.

6.1 TC1: Two-phase shock tube with mass transfer

In this test-case, the shock tube is filled out with liquid dodecane on the left at high pressure $p_l = 10^8$ and vapor dodecane on the right at atmospheric pressure $p_g = 10^5$. Note that, for numerical reasons, each chamber contains a weak volume of the other fluid ($\alpha_k = 10^{-8}$). The diaphragm is located at $x = 0.75$ m (the tube is 1 m long) and the results are shown at a time of $t = 473 \mu s$. The computation are performed by using a 1000 mesh grid.

A comparison between the numerical solutions obtained with and without heat and mass transfer is performed for estimating the influence of these terms. Moreover, results are compared with the ones obtained by Pelanti and Shyue [21] (considering a pressure relaxation coupled with a pressure-thermo-chemical relaxation). These comparisons are reported in Fig. 4.

Looking at Fig. 4, the influence of heat and mass transfer can be observed. In fact, an additional evaporation wave appears between the rarefaction wave (at $0.05 < x < 0.12m$) and the contact discontinuity (at $0.87 < x < 0.9m$) (see Fig. 4c-d). The evaporation wave determines a strong increase of velocity (see Fig. 4b) and an increase of pressure at $0.12 < x < 0.8$ m (see Fig. 4a). Note that this value of pressure corresponds to the saturation pressure.

From the comparison with Pelanti and Shyue [21], a very good agreement can be observed in terms of pressure and mixture density (Fig. 4a-c). The maximum value of velocity obtained by means of the present model is higher than the one obtained in [21] (nearly 7% of difference). Nevertheless, it does agree quantitatively with Saurel et al. solution given in [19] (Fig. 4b). In fact, in terms of vapor mass fraction, Y_v , the three models provide three different results (Fig. 4d).

6.2 TC2: Simoes-Moreira shock tube experiments

This test case reproduce the experiments that have been carried out by Simoes-Moreira and Shepherd [39]. The shock tube is filled out with dodecane on the

left at high pressure and vapor dodecane on the right at low pressure chamber ($p = 10^2$ Pa and 10^{-4} [kg/m³]). The diaphragm is located at $x = 0.75$ m (the tube is 1 m long) and all computations were performed by using a 1000 mesh grid.

The velocity of an evaporation wave that propagates in metastable liquid, is measured for different initial temperatures of liquid dodecane. The pressures before and after the evaporation wave were measured in [39]. The same strategy proposed by Zein et al. [20] is followed here for identifying the pressure value on the left hand side of the shock tube. In particular, the initial pressure is fixed so that the pressure in the state before the evaporation front is equal to the measured value (see Table 7).

The front velocity is computed by measuring the space traced by the evaporation wave at different times. In particular, the evolution of starting point of the evaporation wave at 400 μ s and 500 μ s is observed for all computations.

These results are compared with the experimental data and the results obtained by Saurel et al. [19] and by Zein et al. [20] in Fig. 5. As for [20], these results are closer to the experimental points, by displaying a trend of increase of temperature. Moreover, a better agreement than Saurel et al. [19] can be observed. Nevertheless, an overestimation of the velocity front is obtained. This could be due to a strong influence of the variability of the initial conditions (that are affected by a non-negligible uncertainty) and to the coefficients of the EOS that could influence the computations. Nevertheless, remark that, with respect to the cavitation model proposed in Zein et al. [20], the present model has a lower computation cost as explained in Section 3.3, since it is not necessary to integrate over a fractional hydrodynamic time step. This aspect is highlighted in sections 6.3 and 6.4.

Note also that experimental measurements are affected by an uncertainty, then, it is questionable which numerical solution is the most accurate.

T_l	p_l	p_{exp} (Before evaporation)	u_{EF} (m/s) (Experimental)	u_{EF} (m/s) (Computed)
453	1.5	0.24	0.253	0.23851
473	2.2	0.33	0.309	0.37501
489	3.0	0.44	0.390	0.42073
503	3.9	0.59	0.472	0.55698
523	5.0	0.83	0.648	0.75894
543	7.5	1.19	0.837	0.9548
563	11.0	1.91	1.381	1.6398
573	13.0	2.12	1.578	1.8369

Table 7: Initial liquid temperature on the left side, left liquid pressure, experimental pressure measured before the evaporation front, evaporation front velocity measured and computed front velocity.

6.3 TC3: two-phase expansion tube with mixture initial velocities $v = \pm 2$ m/s

Now, let us consider a tube of unit length, filled out with liquid water of density $\rho_2 = 1150 \text{ kg/m}^3$ at an atmospheric pressure $P = 10^5 \text{ Pa}$. The liquid is assumed to contain a uniformly distributed small amount of vapor, $\alpha_1 = 10^{-2}$ in the whole domain. The liquid temperature is equal to $T_2 = 354.728 \text{ K}$ and hence the vapor density $\rho_1 = 0.63 \text{ kg/m}^3$, by assuming the flow in thermal equilibrium $T_2 = T_1$. The solution is shown at a time $t=3.2 \text{ ms}$ in Fig. 6. The computation is performed by using a mesh of 5000 cells. A velocity discontinuity is set at $x=0.5 \text{ m}$ at initial time. We set $v = -2 \text{ m/s}$ on the left and $v = 2 \text{ m/s}$ on the right of the discontinuity.

As it can be observed in Fig. 6c-d, the vapor volume fraction increase is located in the center of the tube, where a mechanical expansion exists. It corresponds to a region, where the pressure attain the saturation value of about 0.5 Pa (see Fig. 6a). Also in this test case, the comparison with the results obtained by Pelanti and Shyue [21] and by Zein et al. [20], shows a very good agreement in terms of pressure and velocity (Fig. 6a-b). Some differences can be observed in terms of vapor volume fraction and vapor mass fraction, Y_v , (see Fig. 6c-d), for which the present model provides a maximum value that is between those ones obtained by the other two cavitation models.

Nevertheless, as in [21], our results are obtained with a reduction of the computational cost with respect to Zein et al. [20]. In fact, in the case of heat and mass transfer, the CPU time is reduced of nearly 9 times with respect to the method proposed in [20] (with respect to our implementation of the method). In fact, the CPU time is of 2.15 h (32000 time steps and $dt=1.0 * 10^{-7}$) and of 18.838 h (763550 time steps) for our computation and for [20], respectively. Note that computational cost description in [20] makes not possible a more accurate comparison.

6.4 TC4: two-phase expansion tube with mixture initial velocities $v = \pm 500$ m/s

In this section, the analogous test of Section 6.3 but with different initial conditions is presented. In particular, the rarefaction effects are increased by setting the initial velocity $v = -500 \text{ m/s}$ on the left and $v = 500 \text{ m/s}$ on the right. The computation is performed by using a mesh of 5000 cells and the solution is shown at a time $t=0.58 \text{ ms}$ (see Fig. 6).

Since the initial velocity is very large (Fig. 6b), the evaporation is consequently much more intense in the center of the tube, where the vapor volume fraction attains the value of 1 (see Fig. 6c).

The comparison with the results obtained by Pelanti and Shyue [21] and Zein et al. [20] shows a very good agreement in terms of pressure, velocity and vapor volume fraction (Fig. 6a-c). As in the TC3 (see Section 6.3), some differences can be observed in terms of vapor mass fraction, Y_v , (see Fig. 6d). In particular, a difference of nearly 20% can be observed for the maximum. Since no experimental data are available for this test-case, it should be useful to perform a sensitivity analysis by characterizing the amount of uncertainty to consider for the initial conditions.

Also in this test case, a reduction of the computational cost is observed with

respect to Zein et al. [20]. In fact, when considering heat and mass transfer, the CPU time is reduced of nearly 2.5 times with respect to [20]. In particular, the CPU time is of 1.45 h (5800 time steps and $dt=1.0 * 10^{-7}$) and of 3.372 h (186601 time steps) for our computation and for [20], respectively. Note that computational cost description in [20] makes not possible a more accurate comparison.

7 Conclusions and perspective

The present work is devoted to the development of a new cavitation model in order to reproduce compressible two-phase flow with mass transfer. In particular, starting from the model developed in [19] for a five equation model, the present model permits to reduce the computational cost by coupling the treatment of heat and mass transfer terms proposed in [19] for a five-equation model, with the solution admissibility procedure of [21]. This allows to reduce the computational cost by preserving, always, the positivity of solution.

Moreover, the model has been theoretically extended to more complex models, such as the six and seven-equation models, showing the flexibility of the present cavitation model, a good accuracy and a reduced computational cost.

Several results have been presented for highlighting the main contributions of the proposed approach. Well-known numerical configurations used in the literature for assessing robustness of compressible two-phase models have been considered. The proposed method yields very good results in terms of accuracy with respect to the experimental data and numerical solutions known in literature. In some results, the effect of the heat and mass transfer have been assessed and evaluated. In particular, shock tube and two-phase expansion tube problems have been computed. The appearance of the evaporation wave has been observed in the case of pure liquid phase and not-pure phase. The comparison with experimental data and other numerical methods known in the literature [21, 19, 20] showed a very good agreement, thus assessing the proposed model.

Note that for some quantities of interest, slight differences with respect to other numerical solutions have been observed. Since no experimental data are available, it is difficult to determine the reason for this difference. Future works will be oriented towards sensitivity analysis for assessing the influence of initial conditions and empirical coefficients in order to assess the variability of the numerical solution. Other actions will be focused on the extension of the present methods to multi-dimensional problems.

8 Acknowledgement

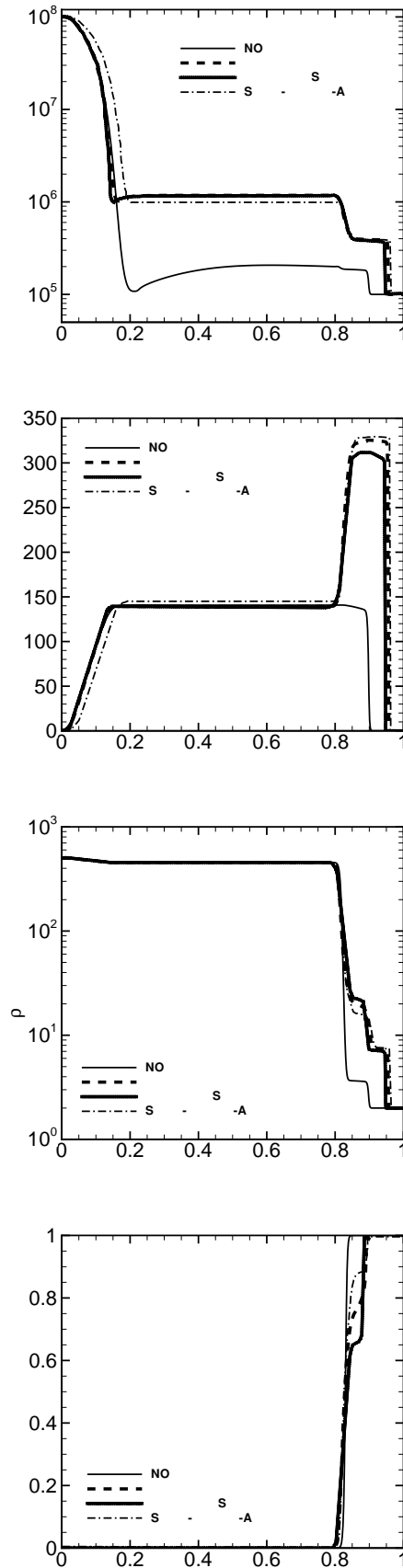


Figure 4: Pressure, velocity, mixture density and $Y = \alpha_1 \rho_1 / \rho$ obtained at a time of $t = 173 \mu s$.

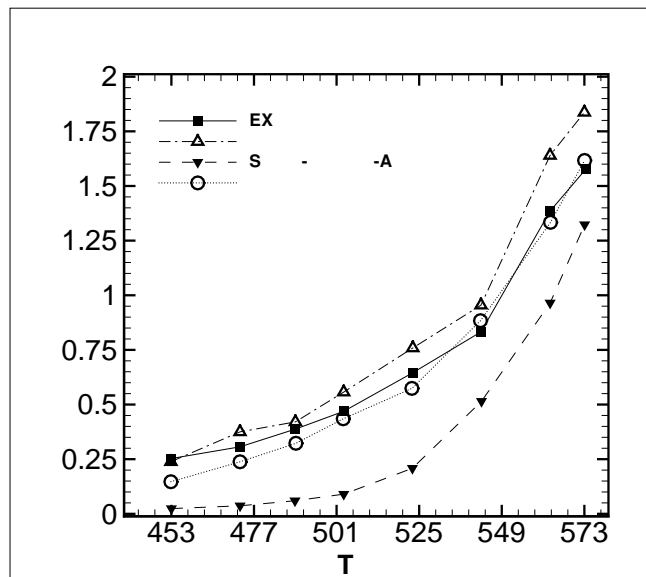
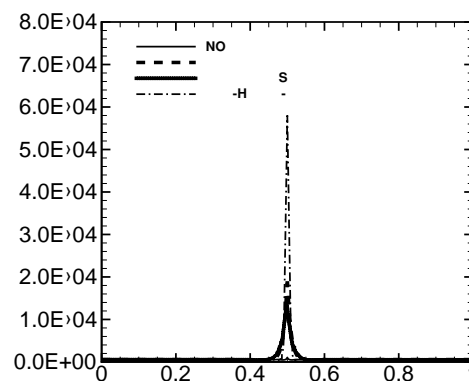
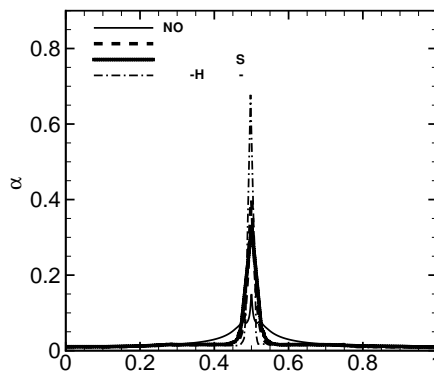
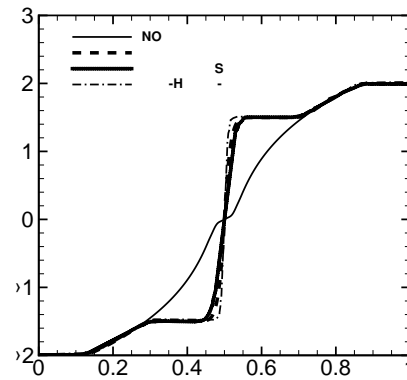
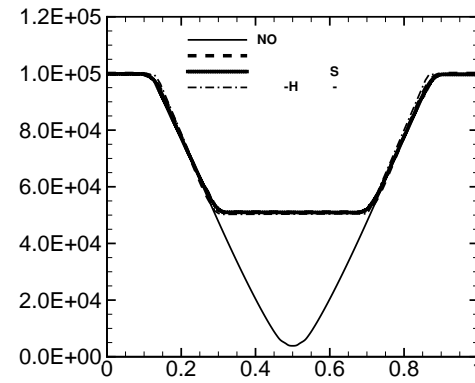
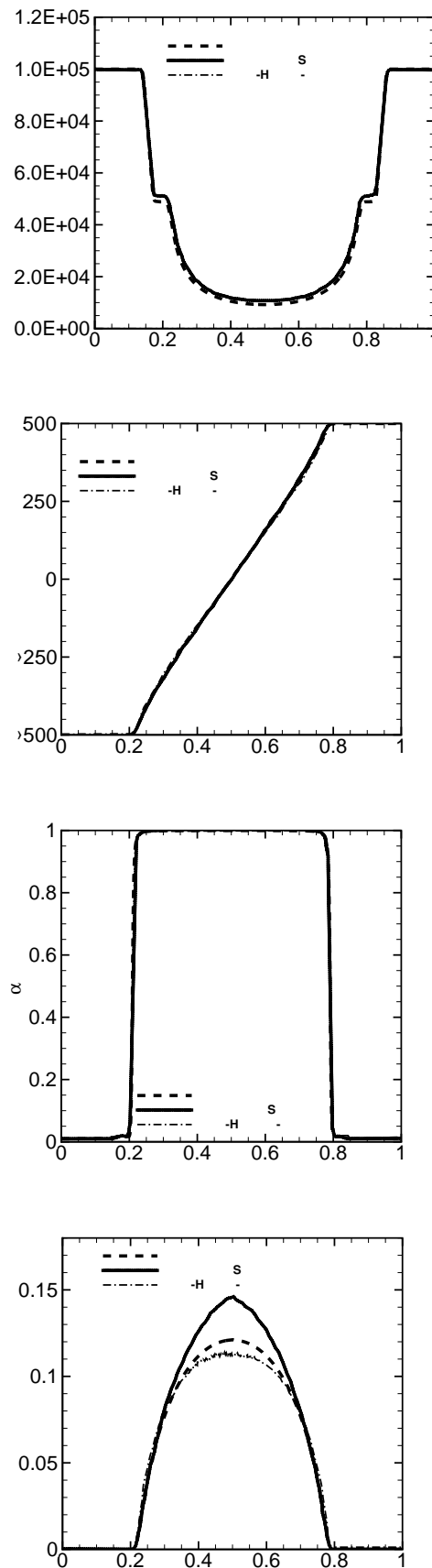


Figure 5: Comparison of the evaporation front velocity obtained for different initial left liquid temperature. The profiles have been obtained experimentally, by the present model, in Saurel et al. [19] and Zein et al. [20].



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Figure 6: Pressure profile, velocity profile, vapor volume fraction and vapor mass fraction $Y = \rho_v \rho / \rho$ obtained at time $t = 3.2$ ms.



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Figure 7: Pressure profile, velocity profile, vapor volume fraction and vapor mass fraction $Y = \rho_v / \rho_c$ obtained at time $t = 0.58$ ms.

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ISSN 0249-6399